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Evaluation of the accuracy of thermal dissociation CRDS and LIF techniques for atmospheric measurement of reactive nitrogen species

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Abstract. The sum of all reactive nitrogen species (NO_y) includes NO_x (NO₂ + NO) and all of its oxidized forms, and the accurate detection of NO_{ν} is critical to understanding atmospheric nitrogen chemistry. Thermal dissociation (TD) inlets, which convert NO_y to NO₂ followed by NO₂ detection, are frequently used in conjunction with techniques such as laser-induced fluorescence (LIF) and cavity ring-down spectroscopy (CRDS) to measure total NO_v when set at >600 °C or speciated NO_{ν} when set at intermediate temperatures. We report the conversion efficiency of known amounts of several representative NO_v species to NO₂ in our TD-CRDS instrument, under a variety of experimental conditions. We find that the conversion efficiency of HNO₃ is highly sensitive to the flow rate and the residence time through the TD inlet as well as the presence of other species that may be present during ambient sampling, such as ozone (O₃). Conversion of HNO₃ at 400 °C, nominally the set point used to selectively convert organic nitrates, can range from 2 to 6 % and may represent an interference in measurement of organic nitrates under some conditions. The conversion efficiency is strongly dependent on the operating characteristics of individual quartz ovens and should be well calibrated prior to use in field sampling. We demonstrate quantitative conversion of both gas-phase N₂O₅ and particulate ammonium nitrate in the TD inlet at 650 °C, which is the temperature normally used for conversion of HNO₃. N₂O₅ has two thermal dissociation steps, one at low temperature representing dissociation to NO₂ and NO₃ and one at high temperature representing dissociation of NO₃, which produces exclusively NO₂ and not NO. We also find a significant interference from partial conversion (5–10 %) of NH₃ to NO at 650 °C in the presence of representative (50 ppbv) levels of O₃ in dry zero air. Although this interference appears to be suppressed when sampling ambient air, we nevertheless recommend regular characterization of this interference using standard additions of NH₃ to TD instruments that convert reactive nitrogen to NO or NO₂.

1 Introduction

The catalytic cycling of nitrogen oxides ($NO_x = NO + NO_2$) plays a key role in the formation of tropospheric ozone (O₃) from the photooxidation of volatile organic compounds (VOCs). Reactive nitrogen species, such as alkyl and multifunctional nitrates (ANs, RONO₂), peroxy nitrates (PNs, RO₂NO₂), and nitric acid (HNO₃) serve as reservoirs and sinks of NO_x. The formation of these species results in a chain termination that determines the efficiency of the O_3 production cycle and can also transport NO_x far from the original emission source. For this reason, total reactive nitrogen $(NO_v = NO + NO_2 + RONO_2 + RO_2NO_2 + HNO_3 +$ HONO + NO₃ + 2× N₂O₅ + aerosol nitrates) is an important tracer in monitoring tropospheric O₃ production. Its accurate detection is critical in field measurements of ambient air quality, as O₃ is a known health risk, and a number of regions across the US are currently in non-attainment or near nonattainment with national ambient air quality O₃ standards (EPA, 2016). However, the sources and fates of NO_{y} species are complex and remain poorly characterized in some regions. Measured total reactive nitrogen has in some cases deviated significantly from the sum of the measured individual components, $\Sigma NO_{v,i}$ (see Fahey et al., 1986; Bradshaw et al., 1998; Neuman et al., 2012; and others referenced within). This unmeasured NO_{ν} , sometimes referred to as "missing NO_v", indicates the need for a more complete understanding of total and speciated reactive nitrogen and for accurate analytical instrumentation for NO_v measurement (Crosley, 1996; Williams et al., 1998; Day et al., 2003).

Techniques that detect the major individual components of NO_v include detection of NO and NO₂ by chemiluminescence (Ridley and Howlett, 1974; Kley and McFarland, 1980), cavity ring-down spectroscopy (CRDS; Fuchs et al., 2009), or laser-induced fluorescence (LIF; Thornton et al., 2000), as well as detection of HNO₃ by chemical ionization mass spectrometry (CIMS; Fehsenfeld et al., 1998; Huey et al., 1998; Neuman et al., 2002; Huey, 2007) or mist chamber sampling (Talbot et al., 1990). Additionally, speciated peroxyacyl nitrates (PANs) have been detected by gaschromatography electron capture detection (Darley et al., 1963; Flocke et al., 2005) and CIMS (Slusher et al., 2004), while N2O5 and ClNO2 have been detected by CRDS (Dubé et al., 2006; Thaler et al., 2011) and CIMS (Kercher et al., 2009). HONO has been detected by long path differential optical absorption spectroscopy (Perner and Platt, 1979), and NO₃ has been detected by CRDS (King et al., 2000). However, fewer methods have been developed for detection of the broad suite of individual alkyl and multifunctional nitrates, which have been suggested to comprise upwards of 20% of NO_v in the mid-latitude continental boundary layer and may be higher in remote locations (O'Brien et al., 1995; Day et al., 2003; Worton et al., 2008; Beaver et al., 2012; Xiong et al., 2015; Lee et al., 2016). An alternative to detecting individual components of NO_{y} is the use of a molybdenum oxide or gold catalyst in the presence of CO to reduce all NO_{ν} species to NO, followed by NO detection by chemiluminescence (Winer et al., 1974; Fahey et al., 1986), though catalyst-based techniques are known to require frequent cleaning and are potentially sensitive to contamination and to interferences at ambient levels of ammonia, HCN, acetonitrile and R-NO₂ compounds (Crosley, 1996; Kliner et al., 1997; Bradshaw et al., 1998; Williams et al., 1998; Day et al., 2002). An alternative method developed by Day and coworkers (Day et al., 2002) uses a quartz thermal dissociation (TD) inlet to rapidly thermally convert nearly all NO_y species to NO_2 , which is then detected by laser-induced fluorescence. The NO_y species in the TD inlet undergo the following reaction:

$$XNO_2 + heat \rightarrow X + NO_2,$$
 (R1)

where X is HO, RO, or RO₂. Heated inlets had previously been used to dissociate PNs (Nikitas et al., 1997), but the TD inlet developed by Day et al. (2002) takes advantage of the different O-N bond energies of ANs, PNs, and nitric acid to separately and selectively detect these three classes of NO_y. A plot of measured NO₂ signal as a function of inlet temperature (hereafter referred to as a "thermogram") yields a stepwise dissociation curve with increases in signal near 100, 300, and 500 °C, corresponding to the dissociation of PNs, ANs, and HNO₃ respectively. By setting the TD oven temperature to one of the three plateaus, they were able to measure each class of NO_y, by comparison of the NO₂ signal in a given channel to the signal measured at the adjacent lower temperature plateau.

In recent years, a suite of other instruments have incorporated this NO_{ν} TD inlet method into existing techniques that measure NO_2 or the radical co-fragment X in Reaction (R1), such as chemical ionization mass spectrometry (TD-CIMS; Slusher et al., 2004; Zheng et al., 2011; Phillips et al., 2013), cavity ring-down spectroscopy (TD-CRDS; Paul et al., 2009; Thieser et al., 2016), and cavity attenuated phase shift spectroscopy (TD-CAPS; Sadanaga et al., 2016). Each instrument has its own advantages and disadvantages. For example, TD-LIF detects NO₂ at low pressure following thermal dissociation. Secondary recombination reactions of the dissociated radicals would thus be suppressed in the detection region, although the thermal dissociation inlet may be operated at either high or low pressures in these instruments. However, it is subject to interferences from urban levels of NO and NO₂ (Paul et al., 2009; Wooldridge et al., 2010). TD-CIMS can differentiate between the different types of PNs but requires regular calibration of each species, not all of which have native standards readily available. TD-CAPS is subject to interferences from glyoxal and methylglyoxal (Sadanaga et al., 2016). TD-CRDS is an absolute measurement but can be subject to other interferences, as discussed in Sect. 3.

Recent TD inlet studies (Day et al., 2002; Paul et al., 2009; Thieser et al., 2016) have measured the conversion efficiency for several AN and PN species with known concentrations in a laboratory setting. These studies all note the possibility of secondary reactions that either increase or decrease the NO₂ signal. For example, recombination reactions to reform the AN or PN species prior to reaching the detector will result in a negative bias in NO₂ (too little NO₂ measured). Likewise, ambient levels of O₃ in the sampled air may react in the oven with NO to form NO₂, resulting in a positive bias (Pérez et al., 2007), though this reaction rate depends on the TD inlet pressure and flow rate (Wooldridge et al., 2010). Day et al. (2002) found that recombination reactions were significant for PNs but caused minimal problems for nitric acid, since the OH radical is far more likely to be lost to the walls of the oven than to recombine with NO₂. More significant is the reaction of dissociated RO₂ and HO₂ radicals with ambient levels of NO and NO₂. Thieser et al. (2016) parameterized the bias in peroxyacyl nitrate and 2-propyl nitrate detection in their inlet as a function of ambient NO and NO₂ concentrations but noted that these parameterizations may vary for other PNs or ANs. In cases where the concentration of one category of NO_y species far exceeds the others, such as the high HNO₃ : ANs ratios in Pusede et al. (2016), speciated measurements can be significantly affected by biases in measurements of the other NO_y compounds.

A four-channel CRDS instrument (hereby referred to as the NOAA TD-CRDS instrument) for detection of nitrogen oxides was recently developed (Wild et al., 2014). In this instrument, one channel is equipped with a TD inlet set at $650 \,^{\circ}\text{C}$ and is used to measure all NO_v species (including NO₂, as well as NO by chemical conversion with an O₃ addition to NO₂). Two other channels simultaneously monitor NO₂ and NO, and so a measurement of NO₂ (= NO_y - NO_x) can be derived. Because NO is intentionally detected as NO_2 in the NO_{ν} channel, this instrument avoids the majority of the NO \leftrightarrow NO₂ interconversion interferences that affect many other thermal dissociation instruments. Analogous to the studies which measured the conversion efficiencies of ANs and PNs (Day et al., 2002; Paul et al., 2009; Sadanaga et al., 2016; Thieser et al., 2016), we present here an analysis of the conversion efficiencies of several other NO_{ν} species and the interferences that affect the operation of this high temperature inlet. These interferences include the temperature dependence of HNO₃ conversion, which is important to understanding both its quantitative conversion at 650 °C as well as its potential to interfere with measurements of ANs at lower temperatures. We also compare these results to those from the TD-LIF instrument of Day et al. (2002), hereby referred to as the Berkeley TD-LIF instrument. Additionally, we report the temperature dependence of N₂O₅ conversion, which is shown to occur in two steps; first, the conversion efficiency of ammonium nitrate aerosol and finally the interference of NH₃ through its partial conversion to NO.

2 Methods

2.1 Thermal dissociation cavity ring-down spectroscopy (TD-CRDS)

Cavity ring-down spectroscopy is a direct absorption technique for measuring the concentration of trace gases (O'Keefe and Deacon, 1988; Fuchs et al., 2009). The fourchannel 405 nm NOAA TD-CRDS instrument, which has been used by our group in both lab-based studies and atmospheric sampling (Wild et al., 2014, 2016), simultaneously measures ambient NO₂ in one channel, while chemically converting NO and O₃ to NO₂ in the second and third channels, and thermally converting NO_y to NO₂ in a TD oven in the fourth channel. In this study, we have used only the NO_y channel to study the conversion efficiency of several reactive nitrogen species to NO₂. Figure 1 shows a schematic of the relevant instrument plumbing and optical cavity. The details of the optical cavity can be found in Wild et al. (2014); only a brief description of the optical system and the details of the TD inlet that deviate from that study will be described here.

Sampled air is pulled into a 50 cm long high-finesse optical cavity capped by highly reflective end mirrors, with purge flows of 25 sccm (standard cubic centimeters per minute at 273.15 K and 1 atm) added in front of each mirror to maintain mirror cleanliness. The output of a 0.5 nm bandwidth, continuous wave diode laser centered at approximately 405 nm and modulated at 2 kHz is passively coupled into one end of the optical cavity. The laser light builds up in the cavity, and when it is modulated off the decaying output light intensity is monitored by a photomultiplier tube on the far side of the cavity. The measured light decay profiles are summed and fit at a 1 Hz repetition rate to yield the ring-down time τ . The ring-down time is inversely related to the concentration of the absorbing gas, NO₂ in this case, which can be derived as

$$[NO_2] = \frac{R_L}{c\sigma} \left(\frac{1}{\tau} - \frac{1}{\tau_0} \right), \tag{1}$$

where R_L is the ratio of d, the mirror separation length, and *l*, which is the distance over which the sample is present. The speed of light is represented by c, σ is the absorption cross section of NO₂, and τ_0 is the ring-down time of a reference cavity without any absorbing gases, which is obtained by flushing the cavity with an excess flow of zero air for 30s every 10 to 20 min. If purge volumes were not used, the R_L term in Eq. (1) would simply be 1, but, since purge volumes are used here, σ/R_L is characterized regularly by filling the cavity with several different known NO₂ concentrations (obtained by reacting the output of an O₃ standard source with excess NO) and calculating the slope of the measured optical extinction vs. $[NO_2]$ as described in Washenfelder et al. (2011). This value was measured approximately once per month during laboratory tests with this instrument but was constant to within ± 1 %, with an average value of 6.25×10^{-19} cm². More regular calibrations of the σ/R_L value during recent field studies show similar stability. The NO₂ signal can be measured with a lower detection of 18 pptv (1σ) in 1 s (Wild et al., 2014).

The NO_y TD oven inlet consists of a quartz tube (0.39 cm ID and 63 cm in length, of which 38 cm is heated) wrapped in nichrome wire and insulated with fiberglass. The flow rate through the inlet and optical cavity is controlled by a mass flow controller on the downstream side of the optical cavity. Because the standard flow rate is held constant during each experiment, the volumetric flow rate, and therefore the TD residence time, varies with oven temperature. For exam-



Figure 1. Instrument schematic of the TD-CRDS instrument used in this study. An NO_y source (HNO₃ permeation tube, N₂O₅ cold trap, NH₄NO₃ particle atomizer + DMA size selector, or NH₃ permeation tube) is diluted by a zero air flow (with an option for adding O₃, VOCs, RH, or CO through the secondary addition port) and passed through the TD oven. A portion of the flow is sampled prior to entering the oven with one of several types of auxiliary measurements (CIMS for N₂O₅; an ultra-high sensitivity aerosol spectrometer, UHSAS, for NH₄NO₃ particles; or commercial CRDS for NH₃). After flowing through a cooling region, the sample passes through a particle filter and then is mixed with a ~ 30 ppmv addition of O₃ in a mixing volume before entering through the optical cavity, where NO₂ is measured by CRDS.

ple, the 4.5 cm³ inner volume of the oven results in an oven residence time of 30-100 ms at a flow rate of 1.9 slpm (standard liters per minute; at 273.15 K and 1 atm) for temperatures from 25 to 650 °C. A flow rate of 1.9 slpm represents the normal operating conditions of this instrument, but flow rates between 0.25 and 3 slpm were tested, which provides oven residence times between 20 and 400 ms. The temperature of the TD oven is monitored by a thermocouple mounted to the outer side of the quartz tube and therefore is slightly lower than the temperature of the gas. However, inserting a temperature probe into the inner part of the TD inlet yields a temperature profile, shown in Fig. S1 in the Supplement, which approaches the temperature set point by the end of the inlet. All oven temperatures described hereafter refer to the measured thermocouple temperature. After passing through the TD oven, the gas cools to room temperature in the nonheated portion of the quartz tube, passes through a particle filter (47 mm diameter, 1 µm pore size PTFE membrane) to remove non-volatilized particles, and then enters a $15 \,\mathrm{cm}^3$ mixing volume prior to entering the CRDS cavity. There, O₃ (\sim 30 ppmv after dilution) is added to the sampled air to convert any NO that formed in the thermal dissociation to NO₂. As the rate constant for the NO + $O_3 \rightarrow NO_2 + O_2$ reaction is more than 3 orders of magnitude faster than the NO₂+O₃ \rightarrow $NO_3 + O_2$ reaction, conversion of NO_2 to NO_3 (and subsequently to N_2O_5) is at most 1–2 % in this mixing volume and is corrected for using a previously described method (Fuchs et al., 2009). To measure the thermograms shown in this paper, the oven temperature was set to a sequence of temperatures spanning 300 to 650 °C and spaced by 25 °C in a random order. The measured NO_2 concentrations are averaged at each temperature set point for approximately 10–15 min.

2.2 NO_y samples and additions

Samples of reactive nitrogen species (labeled as " NO_{ν} source" in Fig. 1) were introduced into the TD oven in several ways. HNO₃ and NH₃ were obtained by passing a 50 sccm flow of zero air through a calibrated 45 °C permeation tube containing HNO₃ (VICI Metronics) or NH₃ (KinTek), providing gaseous outputs of 64 and 23 ng min⁻¹, respectively (Neuman et al., 2003). Subsequent dilution in 0.5-4 slpm zero (synthetic) air resulted in HNO3 and NH3 concentrations of 5 to 40 ppby. Because both these species readily adsorb to instrument surfaces (Neuman et al., 1999), only fluorinated ethylene propylene (FEP) Teflon tubing was used between the permeation tube and the TD oven, and all tubing was kept as short as possible (typically less than 30 cm) and was wrapped in 100 °C heating tape to reduce losses to the walls. However, these precautions were found to be unnecessary in this laboratory study, since the constant flow from the permeation tube resulted in an equilibrium in which the adsorption losses to the walls were equal to the rate of offgassing.

NO was obtained by dilution of the output of a calibrated standard (Scott-Marrin, 0.2 % in N2). N2O5 was synthesized via a procedure adapted from Davidson et al. (1978) and Bertram et al. (2009), which has been used as a calibration for the N₂O₅ channel of a CRDS NO₃ instrument (Dubé et al., 2006; Wagner et al., 2011). Pure samples of NO and O₂ were mixed to yield NO₂, and this mixture was reacted in a flow tube with excess O₃, yielding NO₃ which then reacted with NO₂ to form N₂O₅. The resulting mixture flowed through a glass trap at -78 °C, where N₂O₅ solidified as a white crystal. A gaseous sample of N₂O₅ was obtained by flowing 20–50 sccm of zero air over the solid –78 °C sample and then diluting further in zero air. Gas-phase N₂O₅ prepared in this way is known to contain variable but significant amounts of HNO₃ (Bertram et al., 2009), and thus efforts were made to minimize this interference by baking all glassware for several hours before use and by distilling the solid N₂O₅ sample regularly by bringing it to room temperature under an O₃ flow for 10 min. Nevertheless, some HNO₃ was always present in the sample, and therefore the output of the trap was passed through a nylon wool scrubber prior to entering the TD oven, which removed HNO₃ without significantly perturbing the N₂O₅ concentration. Finally, ammonium nitrate particles were generated by running a 0.1 g L^{-1} solution of aqueous NH₄NO₃ through an atomizer and size-selecting particles of a certain diameter with a custom-built differential mobility analyzer (DMA). Conductive tubing, rather than Teflon, was used to minimize electrostatic build-up and loss of particles to the walls before entering the TD oven.

In order to test whether common atmospheric gases would interfere with the conversion efficiency, some additional species were added to the sample prior to entering the oven. Water was added by passing the dilution zero air through a water bubbler prior to mixing with the HNO₃ sample. Various amounts of O₃ were added by running the dilution zero air through an O₃ calibrator (Thermo Fisher Scientific 49i) that is also capable of generating up to 200 ppm O_3 in 1–3 slpm of zero air. We also investigated the effect of various VOCs, including a high concentration of propane (~ 5 ppmv) and a standard mixture of VOCs (Air Liquide) consisting of *n*-hexane (1.234 ppm), propanal (0.397 ppm), 2-butanone (1.237), benzene (1.151 ppm), methylcyclohexane (0.938 ppm), ethylbenzene (1.213 ppm), 2,2,4-trimethylpentane (1.186 ppm), isopropyl benzene (1.148 ppm), and ethanol (0.994 ppm). This mixture is commonly used to calibrate gas chromatography-mass spectrometry (GC-MS) instruments but here provides common atmospheric species with a range of masses, bond strengths, and degrees of oxidation. It was diluted to 50 ppbv total VOCs by addition of zero air prior to entering the oven. We also added CO in varying quantities to the HNO₃ and NH₃ samples.

2.3 Ancillary measurements

Several instruments were used as ancillary confirmation for some of the NO_{ν} sample concentrations. In each case, a Teflon tee split the sample input and a portion of the flow was pulled into the secondary instrument prior to entering the TD oven, as shown in Fig. 1. In the case of NH₃, a Picarro G2103 NH₃ analyzer with a manufacturer's specified 1 ppbv detection limit at 5 s integration time was used. A custombuilt iodide adduct chemical ionization mass spectrometer (Lee et al., 2014), described in further detail in Veres et al. (2015), was used to monitor the N2O5 and HNO3 concentrations from the N₂O₅ solid sample prior to dissociation in the oven. In this instrument, N₂O₅ and HNO₃ mixed with I⁻ ions produced by passing CH₃I through a ²¹⁰Po source, and the resulting $HNO_3 \cdot I^-$ and $N_2O_5 \cdot I^-$ ions were detected by quadrupole mass spectrometry at m/z = 190 and 235. This measurement has a detection limit of 4 pptv and 70 pptv and error bars of 25 and 25 % (3 σ) for N₂O₅ and HNO₃, respectively. Lastly, an ultra-high sensitivity aerosol spectrometer (Droplet Measurement Technologies) was used to monitor the size distribution of the size-selected ammonium nitrate particles (Cai et al., 2008).

HNO₃ and NH₃ conversion efficiencies were also tested using ambient air for dilution (rather than synthetic air), as sampled during daytime in August 2016 in Boulder, CO. Ambient air was drawn into the two of the four channels of the NOAA TD-CRDS instrument, through two side-byside identical quartz ovens heated to 650 °C at a flow rate of 1.4 slpm, and the output of either the NH₃ or HNO₃ permeation tube was inserted directly into the exposed inlet of one of the ovens, for a duration of approximately 6 min. The NO₂ signal was measured by one of the remaining channels in the NOAA TD-CRDS instrument, and the conversion efficiency of each species was calculated by comparing the difference in NO_2 signal between the two ovens relative to the calibrated output of the permeation tube to correct for small differences in NO_2 signal between the two ovens.

We also present results measured in the Berkeley TD-LIF instrument. It is described in greater detail elsewhere (Day et al., 2002), but briefly HNO₃ and *n*-propyl nitrate samples were provided by permeation tubes similar to those described in Sect. 2.2, diluted in dry zero air, and passed through 20 cm heated length quartz ovens, held at ambient pressure, at a flow rate of 2 slpm. This resulted in residence times of approximately 50 ms. The NO₂ released in the thermal conversion was supersonically expanded into the detection region and measured by laser-induced fluorescence from an individual rovibronic NO₂ line. The NO_y conversion ratio was calculated as the measured NO₂ concentration relative to the maximum NO₂ signal at high temperatures, as the oven temperature was changed at a rate of -10 °C per minute.

2.4 Box modeling

A simple kinetic box model was used to support the experimental findings. Reaction rates for ~ 60 reactions possibly involved in the dissociation and secondary chemical reactions of each NO_{ν} species (listed in the Supplement) were obtained from the Jet Propulsion Laboratory (JPL) Kinetics Database (Sander et al., 2011) and the NIST Chemical Kinetics Database (Manion et al., 2015) at temperatures spanning the 25-650 °C range of the experimental thermograms. For every HNO₃, N₂O₅, and NH₃ thermogram, a simulation was run at each temperature, assuming a starting concentration of the NO_{y} species equal to that observed in the experiment and lasting the duration of the residence time in the oven. The simulation was then allowed to keep running at room temperature for an additional ~ 1 s to mimic the conditions between the oven and the instrument. During this additional low temperature time, 30 ppmv of O3 was added to the simulation to convert NO to NO₂ as in the TD-CRDS instrument. The final concentration of NO_2 at the end of the simulation was recorded for each temperature, which resulted in a simulated thermogram. Several simplifying assumptions were made here. We assume instantaneous heating and cooling of the sample and a uniform temperature profile along the 38 cm length of the TD oven. We also only consider gas-phase reactions and neglect any surface-mediated reactions. When possible, JPL-recommended values for the rate constants were used, but many of those listed did not span the full temperature range of the thermograms. When JPL values were not available, reaction rates from the NIST database were used (see Table S1). We also derive temperature-dependent wall loss constants for O and OH using the procedure outlined by Thieser et al. (2016), but we find that better agreement in some simulations can be achieved with the experimental data by using an empirical value or no wall loss at all. As can be seen in Sect. 3, these simulations successfully replicated a major portion, but not all, of the experimental results, likely due to these simplifications.

3 Results

3.1 HNO₃ thermograms

Figure 2 shows the conversion efficiency of HNO₃ to NO₂ as a function of temperature for several flow rates through the NOAA TD-CRDS. Conversion efficiency was calculated as the measured NO₂ mixing ratio divided by the input HNO₃ mixing ratio. The box model simulations for each flow rate are shown as solid lines of corresponding color. The HNO₃ permeation tube has a calibrated output of $64 \,\mathrm{ng}\,\mathrm{min}^{-1}$, which corresponds to an expected HNO3 concentration of between 5 and 40 ppby, depending on the zero air dilution required for each flow rate. The output of the permeation tube was found to contain approximately 2.5 % NO₂, and all HNO₃ thermograms have had this 2.5% baseline signal subtracted. At a flow rate of 1.9 slpm (where the oven residence time is 30-100 ms depending on temperature), we observe 100 % conversion of HNO₃ at oven temperatures above 600 °C, whereas the thermograms obtained at 1 and 3 slpm reach a maximum conversion of 100% at 550 and 650°C, respectively. The 0.5 slpm thermogram has a slightly lower maximum conversion efficiency (95%), possibly due to the recombination reaction of OH and NO2 during the extended time in the "cooling region" prior to detection.

The box model simulations in Fig. 2 mimic the shape of the experimental data, but some are slightly shifted to higher or lower temperatures, likely because the simulation is extremely sensitive to the flow rate and may be affected by the simplifying assumptions detailed in Sect. 2.4. The shape of the simulated thermogram is entirely controlled by the reaction rate of the initial dissociation reaction of HNO3 to NO2+OH. This reaction has a third-order rate constant of $k_0(T) = 1.82 \times 10^{-4} \times (T/298)^{-1.98} \times e^{(-24\,004/T)}$ and a high-pressure limit of $k_{\infty}(T) = 2 \times 10^{15} \times e^{(-24054/T)}$ (Glänzer and Troe, 1974), and thus at a midrange temperature, such as 500 °C, the HNO₃ lifetime is approximately 250 ms. The inner volume of the oven is 4.5 cm^3 , and so at a flow rate of 1.9 slpm, the gas has a plug flow residence time of 38 ms in the 500 °C oven, compared to a residence time of 77 ms at 1.0 slpm and 153 ms at 0.5 slpm. The simulated conversion efficiency in these midrange temperatures is therefore extremely sensitive to the flow rate, in agreement with our experimental results. However, the experimental 100 % conversion efficiency at high temperatures indicates that there is virtually no recombination of OH and NO₂ once formed, because the recombination rate for $OH + NO_2$ is quite low and because OH radicals are far more likely to be lost to the walls of the oven at a diffusion-limited rate determined by Day et al. (2002) of



Figure 2. HNO₃ thermograms measured at several flow rates in the NOAA TD-CRDS. Conversion efficiency is calculated as measured NO₂ signal relative to the expected concentration of HNO₃. Parentheses in the legend indicate the range of residence times experienced by the sample in the heated inlet. The grey dashed lines indicate 0 and 100 % conversion. Solid lines show simulations using a simple kinetic box model, as described in the text.

 \sim 46 s⁻¹ for 1/4 in (0.63 cm) OD tubing, which is far higher than the pseudo-first-order recombination rate coefficient of 0.075 s^{-1} at [NO₂] = 10 ppbv. No attempt was made to dilute the output of the HNO₃ permeation tube any further, as recombination effects would likely only be less important at lower starting HNO₃ concentrations. Similarly, increasing the starting NO₂ concentration, to mimic conditions in highly polluted environments, was not attempted in this set of experiments, but increasing the starting NO₂ concentration in the kinetic model up to 50 ppbv shows that there is no recombination expected even with elevated NO₂ in the oven. This is in contrast to ANs and PNs, for which the reaction of the dissociated peroxy and alkyl radicals with NO2 is a significant interference (Thieser et al., 2016), but in good agreement with the HNO₃ results of Day et al. (2002) and Sobanski et al. (2016).

At a flow rate of 1.9 slpm, we observe a $\sim 6\%$ conversion of HNO₃ to NO₂ at an oven temperature of 400 °C. Although this efficiency is specific to the conditions of the oven used here, it is a key finding since 400 °C is in the vicinity of the temperature set point chosen for selective detection of total alkyl and multifunctional nitrates by TD-LIF (Day et al., 2002) and other TD instruments. This result is in good agreement with Thieser et al. (2016), who found a $\sim 10\%$ HNO₃ conversion at 450 °C. Sadanaga et al. (2016) report a \sim 15 % HNO₃ conversion at 360 °C at a TD residence time of 3.4 s, which exceeds the range of our study but follows the trend in Fig. 3. In a previous study (Wild et al., 2014), we presented thermograms designed to demonstrate quantitative conversion efficiency at high temperatures. The temperature dependence of thermal conversion was not well constrained at lower temperatures and showed, for example, 30 % conversion at 400 °C. As discussed by Sobanski et al. (2016), the large conversion efficiency presented by Wild et al. (2014) at this temperature is likely incorrect. The extent of HNO₃ con-



Figure 3. Conversion efficiencies of HNO₃ to NO₂ plotted as a function of plug flow residence times in the oven (see text) for five different temperatures. Values were obtained by scaling the measured conversion efficiency in Fig. 1 to the overall maximum and minimum of the thermogram, to account for slight differences between thermograms. Solid circles indicated measurements at ambient pressure, whereas open circles indicate measurements at low pressure. Different line traces indicated different temperatures. A temperature set point between 350 (short dashed line) and 450° (long dashed line) and a residence time less than 200 ms are the conditions normally selected for selective detection of alkyl nitrates with no detection of HNO₃. However, under these conditions HNO₃ conversion may be anywhere between 1 and 30 %.

version is dependent on the residence time in the oven, but because residence time for a given flow rate changes with oven temperature, it is easier to observe this effect by plotting conversion efficiency versus residence time, as in Fig. 3, for five different temperatures (350, 400, 450, 500, and 600 °C). This plot represents transects through Fig. 2 at these five temperatures. Figure S2 shows a log scale plot to highlight the low conversion efficiency region. Most instruments utilizing the TD oven technique use a set point between 350 and 450° and a residence time between 30 and 100 ms to selectively detect ANs and not HNO₃ (Day et al., 2003; Paul et al., 2009; Thieser et al., 2016), but Fig. 3 demonstrates that there is significant variability in the HNO₃ conversion efficiency that depends nonlinearly on oven residence time.

We further measure the effect of pressure on the conversion by placing a heated stainless steel needle valve in front of the oven, thus lowering the pressure inside the oven to 250 mbar. The low pressure transects for each of the five temperatures can be seen in open circles in Fig. 3, and the full thermograms are displayed in Fig. S3. The low pressure transects are slightly lower than those at ambient pressure for the 450 and 500 °C set points but match reasonably well at low and high temperatures, indicating that the onset and final conversion of HNO₃ are not strongly sensitive to pressure. To ensure that HNO₃ was not lost on the walls of the stainless steel valve, the conversion efficiency was measured with the valve fully open and was found to match that taken with no valve. These experiments demonstrate the importance of verifying that a given temperature set point and that flow rate is suitable for measurement of alkyl nitrates without interference from HNO₃ conversion.

To demonstrate the variability within individual TD ovens, an example of the HNO₃ conversion efficiency near the alkyl nitrate temperature set point, as measured by the Berkeley TD-LIF instrument, is shown in Fig. 4. This inlet's alkyl nitrate set point temperature was chosen to be just past the plateau in the *n*-propyl nitrate signal at 410 °C. The HNO₃ conversion to NO_2 was found to be 2.5 %, which for most TD-LIF experiments would be negligible compared to other uncertainties in measured ANs $(\pm 15\%)$ and no correction would be applied. One example where a correction was significant was for the NASA DISCOVER-AQ California deployment, which took place in California's central valley during a period of high NH₄NO₃ aerosol loading. Ratios of $(HNO_3 + NH_4NO_3)$ to ANs were high enough that a correction was necessary and applied to both observations (Pusede et al., 2016). As HNO₃ is derived by subtraction of the ANs, any HNO₃ conversion at the AN temperature results in a high bias for ANs and an equal low bias for HNO₃. The sum of the two remains correct, independent of the onset of the HNO₃ conversion. The Berkeley group has found the HNO₃ conversion to be oven dependent even for identical pressure and flow conditions, indicating that some but not all ovens have impurities at the walls that effectively catalyze HNO₃ decomposition. Ovens with high HNO₃ conversion efficiencies at low temperatures were discarded. These results highlight the importance of careful evaluation and calibration of each TD oven, even when the inner volumes and flow rates are similar.

3.2 HNO₃ thermograms with additions

Tests for other interferences to HNO3 and AN measurements included adding several different chemical species to the HNO₃ sample prior to entering the oven. These were designed to test the hypothesis that certain trace gases found in ambient air would interact with radicals in the oven or would themselves dissociate to form radicals which could react with NO, NO₂, OH, or HNO₃. The results are shown in Fig. 5. In Fig. 5a, a portion of the dilution air was passed through a distilled water bubbler prior to diluting the HNO₃, bringing the relative humidity up to 66%. The change in RH does not alter the shape, onset, or total conversion efficiency of the thermogram. This is to be expected, as the oven temperature is not high enough to dissociate H_2O to OH + H, and reactions between H₂O and the relevant species formed in the oven from HNO3 dissociation are far too slow to be important here. However, it should be noted that both H₂O and HNO₃ are sampled in this experiment at a steady concentration, and it is possible that, during ambient sampling, rapid changes in the RH or HNO₃ concentration could change the overall efficiency. Additionally, we did not test the conversion efficiency at very high RH levels, and it is possible there could be a nonlinear effect of water. Figure 5b shows the



Figure 4. HNO₃ and *n*-propyl nitrate thermograms taken with the Berkeley TD-LIF instrument used in the NASA DISCOVER-AQ California mission. (b) Only HNO₃ with the *y* axis expanded to illustrate the dissociation onset. The oven is from the instrument's alkyl nitrates channel. The flow rate was approximately 2 slpm, and the measurement set point was $410 \,^{\circ}$ C. The dataset was corrected for the 2.5 % dissociation of HNO₃ in the alkyl nitrates channel. A different oven was used for HNO₃ at a set point of 620 $^{\circ}$ C.

measured thermogram with the addition of \sim 50 ppbv VOCs (described in Sect. 2.2) with and without the addition of 90 ppbv O_3 as well as the addition of 5 ppmv of propane, to mimic conditions found in highly polluted wintertime atmospheres. If organic radicals were produced thermally in the TD oven, they could potentially react with NO₂, thus altering that signal. However, the bond dissociation energy of the C-H or C-C bonds most likely to thermally dissociate in each of the VOCs are all significantly higher (typically > 100 kcal mol⁻¹) than that of the O-N bond in HNO₃ $(\sim 50 \text{ kcal mol}^{-1})$, making it unlikely that organic radicals are formed inside the oven from dissociation of VOCs. Reactions of unsaturated hydrocarbons with O atoms or OH radicals tend to be rapid and would produce organic radicals, but these tend to be unstable, and any stable radicals would likely only react with NO₂ to form ANs or PNs. The oven is set at sufficiently high temperatures to dissociate ANs and PNs back to NO_2 + the organic radical. Addition of these VOCs does not affect the measured conversion efficiency, even in the presence of ambient levels of O₃. Ozonolysis of the unsaturated hydrocarbons is slow enough (typically on the order of 1×10^{-17} cm³ molecule⁻¹ s⁻¹) to not have any effect here (we would expect < 0.0001 % reaction for the duration of the oven residence time). An extremely high concentration of propane also has no effect on the overall conversion efficiency, within the error bars of the measurement, for the same reasons as detailed above.

Figure 5c shows the addition of both small and large quantities of O_3 to the HNO₃ sample. Small quantities do not change the onset or overall conversion efficiency, but larger amounts of O_3 reduce the conversion efficiency at high tem-



Figure 5. HNO₃ thermograms (1.9 slpm, ambient pressure) taken with the NOAA TD-CRDS, with various additions added prior to the TD oven. In each frame, the black solid circles indicate the case without additions. (**a**, **b**) No effect is observed when the thermogram is taken at high relative humidity or when VOCs are added. (**c**) Varying amounts of O_3 were added, ranging from ambient levels (75 ppbv) to extremely polluted levels (1200 ppbv), which decreases the overall conversion at high temperatures. (**d**) The addition of 400 ppmv CO alters the shape of the thermogram.

peratures. The kinetic box model does not predict this reduction, as it predicts 100 % conversion efficiency to NO2 at all O₃ levels. The dominant bimolecular reaction of O₃ in the model is the reaction with NO₂ to make NO₃, but, since these reactions are occurring at high temperature, any NO₃ formed will immediately dissociate to NO₂ (see Sect. 3.3). O_3 also thermally dissociates to $O + O_2$ at temperatures above 200 °C (see Fig. S4), but the dominant fate of the O radicals should be loss to the walls. Of the O atoms that are not lost to the walls, their primary reaction is also with NO₂ to form either $NO + O_2$ or NO_3 , but NO should be converted back to NO₂ after the oven. Nevertheless, there is an apparent reduction in the conversion of HNO₃ to NO₂ with increasing O_3 . While the O_3 concentration range in Fig. 5c exceeds that found in ambient air, highly polluted areas may have large enough O₃ concentrations to make this reduction in conversion efficiency significant. Finally, the addition of 400 ppmv CO in Fig. 5d has a marked effect on the onset, shape, and final conversion of the HNO3. This addition was tested because gold catalytic NO_v converters require a 1 % CO addition to drive the dissociation forward. We find that ~ 0.5 % CO is sufficient to promote HNO₃ dissociation even in the absence of a gold catalyst. However, our kinetic model does not replicate the results of the CO addition. Since the ratelimiting step in these thermograms is the initial dissociation of HNO₃, it is unlikely that the reaction between CO and OH or NO₂ plays a role here. It must therefore be caused by a reaction which changes the rate kinetics of the initial dissociation step. However, to our knowledge there have been no laboratory kinetics studies on the CO + HNO₃ reaction. It is likely that there is some surface reaction that affects the HNO₃ conversion in the presence of CO.

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We also note that previous work on TD ovens (Day et al., 2002; Thieser et al., 2016) has cautioned that the elevated temperature of the oven may accelerate the reaction between ambient levels of NO and O₃ to generate NO₂, thereby creating an NO₂ signal that is in fact due to ambient levels of NO. This issue does not affect the TD-CRDS NO_{y} detection scheme, as excess O₃ is intentionally added to the mixing volume after the oven to convert NO to NO₂ to measure total NO_v. Nevertheless, we have investigated how NO responds in the oven, and the results are shown in Fig. S5. A 15 ppbv NO sample was passed through the oven. When no excess O_3 is added to the mixing volume, no NO₂ signal is seen, and, when mixing volume O₃ is added, full conversion of NO to NO₂ is observed, as expected. However, when 100 ppbv of O_3 is added to the oven (with no mixing volume O_3 addition), an approximately 2.2 ppbv NO₂ signal was observed, or a 15% conversion. This is consistent with the kinetic rate expressions for $NO + O_3$ and NO + O, but we do not differentiate between these two mechanisms in these experiments, as O₃ will always form O at the elevated oven temperatures.

3.3 N₂O₅ thermograms

Figure 6 shows the measured thermogram of N_2O_5 in the NOAA TD-CRDS at ambient pressure and flow rates of 1.9 and 1.0 slpm, with the kinetic model simulations for each flow rate shown in solid and dashed lines. Two distinct dissociation steps are observed and confirmed by the kinetic model: one between 30 and 110 °C corresponding to the dissociation of N₂O₅ to NO₂+NO₃ and one above 300 °C corresponding to the dissociation of NO₃. The N₂O₅ synthesis method also produces HNO₃ (Bertram et al., 2009), and, because the bond enthalpies of NO₃ and HNO₃ dissociation are similar (both $\sim 50 \text{ kcal mol}^{-1}$), the thermograms of these two species are expected to overlap at high temperatures. Thus, a nylon wool scrubber was used to remove HNO₃, and the scrubbed sample was simultaneously monitored with an iodide chemical ionization mass spectrometer, described in Sect. 2.3, to ensure the HNO₃ (and not the N_2O_5) was completely removed. The flow rate was lowered to 1.0 slpm in the high temperature scans to accommodate both instruments with a better signal-to-noise ratio. The CIMS measured approximately 120 pptv HNO₃, possibly due to hydrolysis of N_2O_5 after the scrubber, and thus more than 99.5 % of the NO_2 signal we observe is attributed to N_2O_5 .

At high temperatures, each N₂O₅ is expected to produce two NO₂ molecules. Conversion efficiency is calculated from the measured NO₂ concentration relative to the N₂O₅ concentration measured by the CIMS instrument, which samples prior to the TD oven. However, the CIMS instrument requires an empirical calibration factor for any species it measures, and, while the HNO₃ signal may be calibrated using the permeation tube described in Sect. 3.1, there was no independent calibration available for N₂O₅ – only the signal measured using the TD-CRDS instrument. Therefore, the CIMS N₂O₅ signal was assumed to correspond to a 200 % conversion efficiency in the TD-CRDS at 650 °C, and the relative conversion was measured at lower temperatures. The first dissociation step of N₂O₅ to NO₂ and NO₃ is expected at oven temperatures above 110 °C, but, because the sample must then travel through a cooling region prior to entering the CRDS optical cavity (see Fig. 1), approximately 10% of the NO₂ and NO₃ is expected to recombine back to N_2O_5 , based on the rate constant and the residence time in the mixing volume. This behavior has been well characterized previously (Fuchs et al., 2009) and is accounted for in the data analysis, and as expected we observe a 91 % conversion efficiency of N₂O₅ to NO₂ between 110 and 300 °C. At higher temperatures, NO₃ dissociates in the oven before recombining with NO₂, and thus a 200% conversion efficiency is observed. While this is not an absolute measure of conversion efficiency, the relative conversion efficiency is consistent with N₂O₅ dissociation and recombination reaction rates to generate two NO₂ molecules in a distinct stepwise manner. At 150 and 400 °C, the temperature set points often used for detection of PANs and ANs, we find 90 and 105 % conversion of N₂O₅ to NO₂, respectively. The exact values are highly dependent on the residence time in both the oven and in the cooling region but serve to highlight the importance of char-

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acterizing the N2O5 response in every thermal dissociation

oven.



Figure 6. Thermogram of N2O5 measured in the NOAA TD-CRDS at two flow rates. The red squares and red dashed line show the 1.9 slpm thermogram and simulation, while the blue circles and blue solid line show the analogous result at 1.0 slpm. The first dissociation corresponds to $N_2O_5 \rightarrow NO_2 + NO_3$ and the second to $NO_3 \rightarrow NO_2 + O$. The second curve reaches a maximum of 200 %, while the first reaches 90-95 %, depending on the flow rate, due to

detector region. The black dashed line is the experimental HNO3

thermogram from Fig. 2, offset by 100 %. The green triangles in-

dicate measurements of the conversion efficiency without the O₃ addition, confirming that the second dissociation must occur via

 $NO_3 \rightarrow NO_2 + O$ rather than $NO_3 \rightarrow NO + O_2$.

recombination of NO₂ and NO₃ in the cooling region prior to the

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We also measured the conversion of N_2O_5 without the mixing volume O₃ addition at two relevant temperatures in order to determine the mechanism for NO₃ dissociation. These data are shown in green triangles in Fig. 6 and show no difference in onset or maximum conversion efficiency, whether or not mixing volume O_3 is added. As the mixing volume O₃ converts ambient or thermally produced NO to NO₂, the similarity of the two spectra indicates that the NO₃ dissociation mechanism must be $NO_3 \rightarrow NO_2 + O$. However, there are no published rate expressions for this reaction, and the few studies on NO3 thermal dissociation have disagreed about whether the reaction proceeds to NO + O_2 (Johnston et al., 1986) or NO₂+O (Schott and Davidson, 1958). The former argued for the $NO_3 \rightarrow NO + O_2$ mechanism based on thermodynamics, as this reaction is exothermic. However, this implies that NO₃ would be thermally unstable at room temperature, which is not the case. It is likely that there is a significant energy barrier to this reaction. The bond enthalpy of the NO₃ \rightarrow NO₂+O reaction, on the other hand, is $50.4 \text{ kcal mol}^{-1}$, nearly identical to that of $HNO_3 \rightarrow NO_2 + OH$, and the two thermograms are very similar in shape and are centered at the same temperature (500 °C). The simulation shown in Fig. 6 is a fit rate expression of $k(T) = 1 \times 10^{-2} \times (T/298)^9 \times \exp(-1500/T)$ obtained by taking the rate expression of HNO₃ dissociation and iteratively adjusting it until it matched the data. Essentially identical results were observed in the TD-LIF instrument (R. C. Cohen, personal communication, 2016).

3.4 NH₄NO₃ thermograms

NH₄NO₃ particles were generated in situ from an aqueous solution, dried, and size selected by a differential mobility analyzer set at 250 nm prior to entering the TD oven. The conversion efficiency was calculated by comparing the measured NO₂ concentration in the TD-CRDS instrument to the expected number of NH₄NO₃ molecules in the aerosol particles, derived from the number and size of the aerosol particles as measured with an ultra-high sensitivity aerosol spectrometer (UHSAS). The measured UH-SAS histogram was used, along with the literature value for the density of NH₄NO₃, to convert particle diameter to particle volume and then to the total number of NH₄NO₃ molecules. We demonstrate here that the dissociation pathway is $NH_4NO_3 \rightarrow NH_3 + HNO_3$, and we assume that NH_3 is not converted in any significant fraction. A temperaturedependent baseline NO₂ signal is observed when the DMA voltage is set to zero (i.e. when no particles are transmitted), which is attributed to gas-phase HNO₃ molecules which have evaporated from the particles and adsorbed to the tubing walls, and which are subtracted from the total signal. Figure 7 shows the measured thermogram of NH₄NO₃ with the thermogram of gas-phase HNO₃ from Fig. 2 overlaid. The close agreement between the two thermograms demonstrates that the dissociation pathway is $NH_4NO_3 \rightarrow NH_3 + HNO_3$



Figure 7. Measured thermogram of NH_4NO_3 particles as solid circles from the NOAA TD-CRDS. The black solid line indicates the measured thermogram of gas-phase HNO₃ at a 1.9 slpm flow rate (from the gold squares trace in Fig. 2). The close match of these two thermograms indicates that the NH_4NO_3 particles go through HNO₃ as an intermediate and is a good indication that complete conversion is achieved.

and that this reaction is rapid at the temperatures reached in the TD inlet.

For particles that pass through the DMA at a given size set point, the UHSAS measures a size histogram that peaks at a diameter approximately 8% lower, likely because the NH₄NO₃ particles are slightly non-spherical, and therefore the electrical mobility diameter is slightly larger than the geometric diameter. This phenomenon has been discussed at length elsewhere (DeCarlo et al., 2004), and we make no attempt to further characterize NH₄NO₃ particle behavior in the DMA – we have simply taken the UHSAS histogram data to calculate the particle volume, even though this is also subject to slight differences based on the refractive index of NH₄NO₃. However, if the TD oven were to fail to volatilize and convert all NH₄NO₃ particles to HNO₃ and then to NO₂, the measured thermogram would deviate from the HNO₃ spectrum at lower temperatures, where perhaps the heat is not sufficient to drive the NH4NO3 out of the condensed phase. The close match between the two is a good indication that the conversion goes to completion. Additionally, Figs. S6 and S7 show a sample NO₂ measurement measured by TD-CRDS at 650 °C as the particle diameter set point is changed. There is no correlation between particle size and conversion efficiency, indicating that the oven is completely converting all particles without a size dependence.

3.5 NH₃ thermograms

A previous study (Wild et al., 2014) investigated whether ambient levels of ammonia would represent an interference to NO_y conversion and found that it made at most a 1 % difference to the NO_2 signal in dry air, but that this effect was suppressed when RH>10%. We find in the present study that there is a significant interference when ambient levels of both NH₃ and O₃ are present in the oven, but that this effect is potentially suppressed by other species found in ambient sampling. Figure 8 shows a thermogram of NH₃ with and without 100 ppbv O₃ present in the oven. The conversion of NH₃ to NO₂ at 650 °C, calculated as the observed NO₂ signal relative to the added NH₃ concentration, is small without O_3 . This is consistent with the previous study of Wild et al. (2014). However, when 100 ppbv of O₃ is added, the thermogram reaches a maximum molar conversion efficiency of 8 %, with an onset near 400 °C (red circles). In contrast to the HNO₃ thermograms, however, this signal does not appear to plateau at 650 °C but rather continues to grow at higher temperatures. This result is similar to the interference reported by Dillon et al. (2002), which was attributed to a reaction between NH₃ and O₃. The interference is only present when O₃ is added to the mixing volume, indicating that the conversion of NH3 must be producing NO, rather than NO₂, and is subsequently unimportant to instruments that measure NO₂ only, such as TD-LIF instruments. A kinetic model simulation of both experiments is shown in solid lines in Fig. 8. This simulation was carried out with 35 relevant reactions between NH₃, O₃, and the radicals that are formed from these two species in the oven, with the most important reactions listed below. The reaction between NH₃ and O₃ is far too slow to be relevant here, and the oven temperature is not high enough to dissociate NH₃ to NH₂+H $(\Delta H = 108 \text{ kcal mol}^{-1})$. However, O₃ dissociates readily at oven temperatures above 200 °C, and once formed the O atoms may react with NH₃ to form NH₂.

$$\begin{aligned} O_3 &\rightarrow O_2 + O \\ NH_3 + O &\rightarrow NH_2 + OH \\ NH_3 + OH &\rightarrow NH_2 + H_2O \end{aligned} \tag{R2}$$

The reactions of NH₃ are the slowest steps, but once formed NH₂ reacts readily with O atoms.

$$NH_2 + O \rightarrow HNO + H$$

$$\rightarrow OH + NH$$

$$\rightarrow NO + H_2$$
(R3)

HNO then reacts with O, OH, and H to form NO or can also directly dissociate to form H + NO.

$$HNO + O \rightarrow OH + NO$$

$$HNO + OH \rightarrow H_2O + NO$$

$$HNO + H \rightarrow H_2 + NO$$

$$HNO \rightarrow H + NO$$
(R4)

The OH and H atoms formed in reactions (R3) and (R4) then drive Reaction (R2) further. This mechanism takes place entirely in the gas phase and does not take into account any surface-mediated reactions. Many of these reactions have only limited published studies, so the simulation used rate constants that have not been extensively tested. Additionally, to achieve a significant conversion of NH₃ to NO, it



Figure 8. Thermogram of NH₃ taken with the NOAA TD-CRDS, with 100 ppbv of O₃ added before the oven shown as red circles. The blue circle represents an analogous measurement at 650 °C with no O₃ added. Kinetic box model simulations shown in solid lines of corresponding color.

was necessary to decrease the O and OH wall loss constants in the model. This rudimentary simulation predicts the initial signal increase starting at 300 °C, though it has a maximum conversion efficiency of just under 2 %, which is below that observed in the experiment. In Fig. 9, we adjusted the amount of added O₃, while monitoring the conversion efficiency of NH₃ to NO₂ at an inlet temperature of 650 °C. We find that increasing the O₃ increases the conversion, which is consistent with NH_3+O being the limiting reaction to make NH₂. Figure 9 also demonstrates that the conversion of NH₃ is partially quenched by the addition of ambient levels (~100 ppbv) of CO, likely because the $CO + O \rightarrow CO_2$ reaction competes with those in Reaction (R2). Figure 10 shows that the average conversion efficiency of NH₃ when measured in ambient air in Boulder, CO, in August 2016 (which contains 40–60 ppbv O_3 , > 80 ppbv CO_2 , ~15 % RH, and other species) is 0.5 ± 2.4 %, or zero to within the 1σ error from repeated measurements. This is in contrast to the conversion efficiency of HNO₃ in ambient air, shown in the upper right frame of Fig. 10, which is largely unchanged from that measured in zero air. Thus, constituents present in ambient air, such as methane, CO, and water, are possibly suppressing the conversion of NH₃ to NO, likely through the reaction with O atoms.

4 Discussion

Using a thermal dissociation cavity ring-down spectrometer, we have quantitatively added reactive nitrogen species to the TD inlet in order to test the efficiency of the thermal conversion of each species to NO₂ and the effect of any interferences from other trace gases which may be present in the ambient troposphere. We have determined that the TD-CRDS converts HNO₃, N₂O₅, and NH₄NO₃ particles to NO₂ with 100 % efficiency at temperatures above 600 °C, but that the onsets of the dissociation are highly dependent on oven residence time. Despite their similar residence times, the



Figure 9. Conversion efficiency of NH₃ to NO₂ as a function of O₃ added to the TD inlet. Red circles show 10 ppbv NH₃ with O₃ ranging from 0 to 300 ppbv, and the green and blue traces show similar data, but with 100 and 2000 ppbv CO added. The partial depletion of the signal ($\sim 25 \%$) with the addition of CO indicates that the oxygen atoms formed from O₃ pyrolysis are reacting with CO instead of NH₃.

NOAA TD-CRDS and Berkeley TD-LIF instruments measure HNO₃ conversion efficiencies ranging from 2.5 to $\sim 8 \%$ at 410 °C. It is therefore important that the oven residence time is well characterized in instruments designed to selectively detect ANs without interference from HNO₃. Even two TD ovens with identical inner volumes may exhibit different response functions if they have different ratios of surface area to volume.

We find that high levels of ambient O_3 (>500 ppbv) and CO (>400 ppmv) significantly changed the final conversion efficiency and the onset of the conversion, respectively, of the HNO₃ thermogram but that ambient levels of a group of representative VOCs and high RH did not affect the measured thermogram. Modest levels of O₃ converted a portion of NH₃ to NO₂. The conversion mechanism likely arises from a gas-phase reaction between oxygen atoms and NH₃ which produces NO. To our knowledge, the $NH_3 + O_3$ reaction in TD ovens has not been studied in detail, but previous studies of NH₃ conversion in catalytic converters have noted similar results to those presented here – water and CO suppress the NH₃ conversion to NO, while O₃ enhances it (Fahey et al., 1985; Kliner et al., 1997). If not quenched by other species present in ambient air, this effect could represent a potentially significant interference in field sampling for instruments that are sensitive to NO directly or via conversion to NO₂. For example, at 50 ppbv O₃, the 6 % conversion of NH₃ would present an interference of more than 10 % if $NH_3 / NO_v > 1.7$, which is not an uncommon condition in agricultural regions. This signal was suppressed in ambient air, indicating that NH_3 may not interfere with NO_v under most conditions. However, ambient air in Boulder is not representative of all sampling conditions, and, since the species responsible for quenching the reaction remains unclear, more work must be done to better understand the mechanism of the NH_3 / O_3 thermal reaction. This result, along with the others detailed above, serves to emphasize that great care must be taken to characterize the potential interferences in TD NO_y -conversion ovens.

The measured N₂O₅ thermogram exhibits a double dissociation curve, corresponding to the initial dissociation of N_2O_5 to NO_2 and NO_3 and the subsequent dissociation of NO₃. Our results indicate that the mechanism of the second step is $NO_3 \rightarrow NO_2 + O$, in contrast to earlier literature that reported $NO_3 \rightarrow NO + O_2$ as the dominant mechanism. To our knowledge, this is the first published thermogram of NO₃. TD-NO_y instruments often operate in the daytime when N_2O_5 is not a significant fraction of NO_{ν} , though some groups have operated at night and have typically assumed complete conversion to $NO_2 + NO_3$ at the TD inlet set point for PNs (Di Carlo et al., 2013) and complete conversion to $2NO_2 + O$ at the set point for HNO₃ (Wild et al., 2014). These results confirm that there is approximately quantitative conversion at these set points, though there are slight deviations from 100 % conversion near the PN set point. Therefore, care must be taken to select a set point carefully and ensure complete conversion at that temperature. However, this interference would only be significant during nighttime or during very cold weather sampling.

The thermogram of particulate ammonium nitrate matches the thermogram of HNO₃, within the margin of error of the UHSAS measurement. TD ovens have not typically been used explicitly for particle detection, with a few exceptions (Voisin et al., 2003; Smith et al., 2004; Rollins et al., 2010), though very fine particles may be sampled by the inlet, unless they are excluded aerodynamically or physically. These results demonstrate that the volatile portion of the particulate ammonium nitrates will be driven into the gas phase at low oven temperatures, consistent with Rollins et al. (2010), who used a denuder to remove gas-phase nitrates and to detect aerosol organic nitrates in a 325 °C oven. Their results indicate it is likely that particulate organic nitrates would be converted to NO₂ with 100% efficiency in the NOAA TD-CRDS, but this result has not been explicitly tested here. Other NO₃ salts might also be detected via thermal dissociation, although it is expected that they would be nonvolatile at the temperatures of these TD-inlets. Bertram and Cohen (2003) examined NaNO₃ and determined that those particles would not be detected in TD inlets. However, these studies measured pure aerosols, and results may vary with heterogeneously mixed particles with multiple components. The initial dissociation of NH₄NO₃ will produce an NH₃ molecule in addition to an HNO₃ molecule, which means that particles may be subject to the same NH₃ / O₃ interference when sampling in ambient air, which was not considered in this study. Additionally, the particles sampled in this paper were generated and injected directly into the inlet. The efficiency of particle sampling in ambient air will depend on particle size and inlet design, particularly during aircraft measurements. In future studies, a TD inlet that either effectively samples aerosol or effectively excludes aerosol (such



Figure 10. Measurement of HNO₃ and NH₃ conversion in ambient air at an inlet set temperature of 650 °C. (a) Measured conversion efficiencies for standard additions of HNO₃ and NH₃ to the NOAA TD-CRDS inlet sampling ambient air in Boulder, CO, on 9 August 2016. (b, c) Time series of measured NO_y during standard additions. The data are the difference between two NO_y measurement channels, one with and one without the standard addition, to cancel the variation in ambient NO_y during the tests.

as a cyclone), or a combination of the two, could be used to specifically measure aerosol nitrates, which may make up a substantial fraction of NO_y , particularly in polluted wintertime urban atmospheres.

Based on the results of this paper, we make the following three recommendations. (1) TD ovens should be characterized with the appropriate reactive nitrogen compounds regularly at the oven set points using the oven residence time and gas pressure that will be used in ambient sampling. This is especially important given the findings of the Berkeley group regarding impurities found in otherwise identical ovens, as discussed in Sect. 3.1. (2) In addition to the AN and PN calibrations recommended by Day et al. (2002), Thieser et al. (2016), and others, these calibrations should include HNO3. HNO3 calibration will be especially important if sampling in regions where HNO₃ is in large excess over other NO_{v} species. (3) Potential non- NO_{v} species such as NH_{3} should also be regularly introduced into the inlet under conditions where O₃ is present in ambient air to check for potential conversion. These recommendations are similar to those detailed in Bradshaw et al. (1998). The results of Fig. 9 indicate that calibration results may also vary significantly when sampling in ambient air, due to the large number of possible gas-phase reactions available to the wide variety of trace atmospheric species. The last step is particularly important in instruments that detect NO as well as NO₂. Comprehensive calibration of these interferences is key to these instruments' NO_v measurement accuracy, which in turn will provide valuable information about tropospheric NO_x chemistry.

Data availability. Data is available upon requests made to Steven Brown (steven.s.brown@noaa.gov).

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Competing interests. The authors declare that they have no conflict of interest.

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Supplement of

Evaluation of the accuracy of thermal dissociation CRDS and LIF techniques for atmospheric measurement of reactive nitrogen species

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Supporting information



Figure S1. A sample oven temperature profile measured with a 2.0 slpm flow rate through the TD oven inlet, while the oven was set at 650 °C. Distance is measured from end of the quartz tube. The first ~5 cm are not heated, and the heated portion stretched from approximately 5 - 42 cm, with a cooling region from 42 - 63 cm.



Figure S2. Log scale plot of conversion efficiency vs residence time. This plot is similar to the linear plot in Fig. 3, but is presented in log space to highlight small differences in the low conversion efficiency region.



Figure S3. HNO₃ thermograms taken at low oven pressure (~250 mbar). As in Fig. 2, the onset of signal shifts to higher temperatures at faster flow rates.



Figure S4. A simulated O_3 dissociation curve to O. These results indicate that O_3 dissociates to form O at the entire temperature range relevant for AN and HNO₃ TD ovens, but that if allowed to recombine, only ~40% will remain as $O_2 + O$. If wall loss is permitted, nearly all O atoms would be lost to reactions with the wall.



Figure S5. The measured NO₂ mixing ratios as ~15 ppbv NO in zero air is introduced to the NOy thermal dissociation inlet is shown in red. The green and yellow lines represent the addition of O₃ in two places: ppbv levels before the NO sample enters the TD inlet (green) and ppmv levels in the mixing volume just prior to entering the CRDS cavity (yellow). The mixing volume O₃ converts any NO to NO₂ prior to detection, so when this O₃ is added (such as between 4:30 and 5pm), the measured NO₂ is ~15 ppbv, as expected. When O₃ is not added to either the TD inlet or the mixing volume (such as between 4:20 and 4:30pm), no NO₂ signal is observed. However, when O₃ is added to the TD inlet, but not to the mixing volume, and the oven is at 650 °C, (such as between 5:05 and 5:15), approximately 2.25 ppbv NO₂ is observed, indicating that this NO₂ is formed by reaction of O₃ and NO in the oven. This has no effect on this TD-CRDS instrument, as any NO would be converted to NO₂ in the mixing volume region immediately following the TD oven. But techniques such as TD-LIF or TD-CRDS in which NO is not converted to NO₂ would see a ~15% conversion of ambient NO to NO₂, which must be accounted for.



Figure S6. NO_2 signal (red) detected in the NOy channel of the TD-CRDS instrument when NH_4NO_3 aerosol is introduced to the inlets on two separate occasions. The blue trace is the expected NH_4NO_3 concentrations derived from the UHSAS measurement of the particle size distribution. The yellow indicates set DMA diameter.



Figure S7. NO₂ mixing ratios as measured by the TD-CRDS instrument, and derived NO₂ mixing ratios from the UHSAS size distribution of NH_4NO_3 particles, colored by DMA selected diameter. Here, "0 nm" refers to setting the DMA voltage to 0, which nominally does not allow any particles through. A linear trend is shown in the scatter plot, with no dependence on particle size, emphasizing that complete conversion of the NH_4NO_3 particles is observed in the TD oven.



Figure S8. A representative thermogram for each of the four major species studied. All were at ambient pressure and a flow rate of 1.9 slpm, except for the high temperature region of the N_2O_5 trace, which was taken at 1 slpm. The NH₃ thermogram was taken with 100 ppbv of O₃ in the TD inlet.

Table S1. Reactions used in HNO3 box model

Rate laws are presented in table form, where the parameters listed can be inserted into the equation $k(T) = A(298/T)^{n}e^{-(Ea/RT)}$. For third order equations, a high pressure limit is also given. For third order reactions, a value of $F_c = 0.6$ was used. Ea/R is in units of K⁻¹. A is in units of cm³ molec⁻¹ s⁻¹ for second order reactions and cm⁶ molec⁻² s⁻¹ for third order reactions. The rate expression at 298 and 950 K (max and min temperatures used in each thermogram) are given. The technique (experimental, theoretical, combination/review) is given, along with the temperature range and reaction order. Temperature ranges with approximates are based on JPL combinations of multiple studies and are thus approximate.

Reaction	Rate Expression											
	A_0	n ₀	Ea/R ₀	A∞	n∞	Ea/R _∞	Ref.	k(298K)	k(950K)	Technique	Temp range	Order
$HNO_3 \rightarrow NO_2 + OH$	1.83e-4	-1.98	24054	1.26e-15	0	24054	[1]	5.51e-21	409.81	Expt	295-1200	2
$NO_3 \rightarrow NO_2 + O$	*See main text*											
$NO_3 + NO_2 \rightarrow N_2O_5$	2.0e-30	-4.4	0	1.4e-12	-0.7	0	[2]	1.15e-12	5.66e-14	Expt	~250-400	3
$NO_2 + O \rightarrow NO_3$	2.50e-31	-1.8	0	2.2e-11	-0.7	0	[2]	2.74e-12	1.72e-13	Expt	~200-400	3
$NO_2 + OH \rightarrow HNO_3$	1.80e-30	-3	0	2.80e-11	0	0	[2]	9.28e-12	3.29e-13	Expt	~200-600	3
$NO_2 + HO_2 \rightarrow HO_2NO_2$	2.00e-31	-3.4	0	2.90e-12	-1.1	0	[2]	2.53e-12	2.45e-14	Expt	~200-350	3
$NO + O \rightarrow NO_2$	9.00e-32	-1.5	0	3.00e-11	0	0	[2]	1.32e-12	9.33e-14	Expt	~200-500	3
$NO + OH \rightarrow HONO$	7.00e-31	-2.6	0	3.60e-11	-0.1	0	[2]	6.31e-12	2.06e-13	Expt	~200-500	3
$NO + H \rightarrow HNO$	1.22e-31	-1.17	211.6	N/A	N/A	N/A	[3]	1.13e-12	1.57e-13	Review	230-4200	3
$O_3 \rightarrow O + O_2$	7.16e-10	0	11200	N/A	N/A	N/A	[4]	6.49e-7	10000	Review	300-3000	2
$O_2 + H \rightarrow HO_2$	4.40e-32	-1.3	0	7.50e-11	0.2	0	[2]	7.37e-13	5.88e-14	Theory	300-3000	3
$O + H \rightarrow OH$	4.36e-32	-1	0	N/A	N/A	N/A	[5]	8.20e-13	8.55e-14	Review	300-2500	3
$2OH \rightarrow H_2O_2$	6.90e-31	-1	0	2.60e-11	0	0	[2]	5.42e-12	1.06e-12	Expt	~200-700	3
$OH + H \rightarrow H_2O$	4.38e-30	-2	0	N/A	N/A	N/A	[6]	8.28e-11	2.79e-12	Review	300-3000	3
$HO_2 + HO_2 \rightarrow H_2O_2 + O_2$	3.00e-13	0	-460	N/A	N/A	N/A	[2]	0.0858	0.00343	Expt	~250-1200	3
$N_2O_3 \rightarrow NO + NO_2$	1.90e-7	-8.7	4800	4.7e15	0.4	4880	[7]	10000	10000	Review	225-300	2
$HO_2NO_2 \rightarrow HO_2 + NO_2$	4.10e-5	0	10650	4.8e15	0	11170	[8]	0.0738	10000	Expt	260-300	2
HONO \rightarrow OH + NO	1.98e-3	-3.8	25257	1.09e16	-1.23	25016	[3]	1.41e-21	171.88	Review	300-2500	2
$HNO \rightarrow NO + H$	5.48e-7	-1.24	25257	N/A	N/A	N/A	[3]	1.67e-24	1.07634	Review	300-2500	2
$H_2O_2 \rightarrow 2OH$	2.03e-3	-4.86	26820	N/A	N/A	N/A	[5]	3.34e-27	0.00125	Review	500-2500	2
$N_2O_5 \rightarrow NO_2 + NO_3$	1.30e-3	-3.5	11000	9.7e14	0.1	11080	[8]	0.0498	10000	Expt	200-400	2
$HNO_3 + OH \rightarrow H_2O + NO_3$	6.50e-34	0	-1335	2.70e-17	0	-2199	[2]**	1.12e-13	3.95e-14	Expt	~200-350	3
$2NO_3 \rightarrow 2NO_2 + O_2$	8.5e-13	0	2450				[2]	2.29e-16	5.98e-14	Expt	298-329	2
$NO_3 + NO \rightarrow 2NO_2$	1.79e-11	0	-109.45				[9]	2.58e-11	2.02e-11	Review	220-4400	2
$NO_3 + O \rightarrow O_2 + NO_2$	1.00e-17	0	0				[2]	1e-11	1e-11	Expt	298	2
$NO_3 + OH \rightarrow HO_2 + NO_2$	2.2e-11	0	0				[2]	2.2e-11	2e-11	Expt	298	2
$NO_3 + HO_2 \rightarrow O_2 + HNO_3$	3.5e-12	0	0				[2]	3.5e-12	3.5e-12	Expt	298	2
$NO_3 + H \rightarrow NO_2 + OH$	9.4e-11	0	0				[10]	9.4e-11	9.4e-11	Expt	298	2

Reactions used in HNO₃ box model

$NO_2 + O_3 \rightarrow NO_3 + O_2$	1.2e-13	0	2450		[2]	3.24e-17	8.44e-15	Expt	~250-350	2
$NO_2 + O \rightarrow NO + O_2$	5.10e-12	0	-210		[2]	1.03e-11	6.40e-12	Expt	~200-350	2
$NO_2 + HNO \rightarrow HONO + NO$	1e-12	0	1000		[3]	3.49e-14	3.38e-13	Review	300-2500	2
$NO_2 + H \rightarrow NO + OH$	4.00e-10	0	340		[2]	1.28e-10	2.77e-10	Expt	~200-500	2
$NO + O_3 \rightarrow NO_2 + O_2$	3.00e-12	0	1500		[2]	1.96e-14	5.91e-13	Expt	~200-400	2
$NO + HO_2 \rightarrow NO_2 + OH$	3.30e-12	0	-270		[2]	8.16e-12	4.42e-12	Expt	~200-400	2
$O_3 + O \rightarrow 2O_2$	8.00e-12	0	2060		[2]	7.99e-15	8.59e-13	Expt	~250-350	2
$O_3 + OH \rightarrow HO_2 + O_2$	1.70e-12	0	940		[2]	7.26e-14	6.14e-13	Expt	~200-450	2
$O_3 + HNO \rightarrow HONO + O_2$	2.56e-15	3.59	-396.9		[11]	9.48e-15	2.23e-13	Theory	150-1000	2
$O_3 + H \rightarrow O_2 + OH$	1.40e-10	0	470.26		[12]	2.89e-11	8.41e-11	Review	200-300	2
$O_2 + H \rightarrow OH + O$	1.22e-11	0.96	6157.9		[13]	1.30e-20	4.55e-14	Review	950-3550	2
$O + OH \rightarrow O_2 + H$	1.80e-11	0	-180		[2]	3.29e-11	2.19e-11	Expt	~150-500	2
$O + HO_2 \rightarrow OH + O_2$	3.00e-11	0	-200		[2]	5.87e-11	3.72e-11	Expt	~250-400	2
$O + N_2O_3 \rightarrow Products$	4.30e-13	0	0		[14]	4.30e-13	4.30e-13	Theory	199	2
$O + HO_2NO_2 \rightarrow Products$	7.8e-11	0	3400		[2]	8.70e-16	1.96e-12	Expt	225-300	2
$O + HONO \rightarrow OH + NO_2$	2.01e-11	0	3000		[3]	8.58e-16	7.80e-13	Review	300-2500	2
$O + HNO \rightarrow OH + NO$	6.00e-11	0	0		[3]	6.00e-11	6.00e-11	Review	300-2500	2
$O + H_2O_2 \rightarrow HO_2 + OH$	1.40e-12	0	2000		[2]	1.71e-15	1.60e-13	Expt	~275-375	2
$2OH \rightarrow H_2O + O$	1.80e-12	0	0		[2]	1.80e-12	1.80e-12	Expt	250-580	2
$OH + HO_2 \rightarrow H_2O + O_2$	4.80e-11	0	-250		[2]	1.11e-10	6.29e-11	Expt	250-380	2
$OH + HO_2NO_2 \rightarrow H_2O_2 + NO_3$	1.30e-12	0	-380		[2]	4.65e-12	1.96e-12	Expt	~250-325	2
$OH + HO_2NO_2 \rightarrow HO_2 + HNO_3$	1.30e-12	0	-380		[2]	4.65e-12	1.96e-12	Expt	~250-325	2
$OH + HONO \rightarrow H_2O + NO_2$	1.80e-11	0	390		[2]	4.87e-12	1.18e-11	Expt	~275-375	2
$OH + HNO \rightarrow H_2O + NO$	8.00e-11	0	500		[3]	1.50e-11	4.65e-11	Review	300-2000	2
$OH + H_2O_2 \rightarrow HO_2 + H_2O$	2.90e-12	0	160		[8]	1.70e-12	2.44e-12	Expt	240-460	2
$HO_2 + H_2O_2 \rightarrow OH + H_2O + O_2$	1.00e-13	0	0		[15]	1.00e-13	1.00e-13	Theory	825-875	2
$HO_2 + H \rightarrow H_2O + O$	5.00e-11	0	865.95		[6]	2.74e-12	1.96e-11	Review	300-1000	2
$HO_2 + H \rightarrow 2OH$	2.81e-10	0	440.19		[6]	6.42e-12	1.74e-11	Review	300-1000	2
$HO_2 + H \rightarrow O_2 + H_2$	7.11e-11	0	709.6		[6]	6.57e-12	3.29e-11	Review	300-1000	2
$HO_2NO_2 + H \rightarrow Products$	2.46e-14	0	0		[16]	2.46e-14	2.46e-14	Expt	248-315	2
$HONO + H \rightarrow H_2O + NO$	6.39e-13	1.89	1940		[17]	9.43e-16	6.54e-13	Theory	300-3500	2
$HONO + H \rightarrow OH + HNO$	1.26e-11	0.86	2500		[17]	2.86e-15	2.21e-12	Theory	300-3500	2
$HNO + H \rightarrow H_2 + NO$	3.01e-11	0	500		[3]	5.63e-12	1.75e-11	Review	298-2000	2
$H_2O_2 + H \rightarrow OH + H_2O$	1.69e-11	0	1800		[6]	4.04e-14	2.40e-12	Review	300-1000	2
$H_2O_2 + H \rightarrow H_2 + HO_2$	2.81e-12	0	1889.5		[6]	4.96e-15	3.63e-13	Review	300-1000	2
$OH \rightarrow Wall$			40	5 s ⁻¹			**Se	e main text		
$O \rightarrow Wall$			7() s ⁻¹			**Se	e main text		
$C_3H_8 + O \rightarrow C_3H_7 + OH$	1.37e-12	2.68	1870.2		[18]	2.54e-15	3.67e-12	Review	300-2500	2
$C_3H_8 + H \rightarrow C_3H_7 + H_2$	4.23e-12	2.54	3400		[18]	4.64e-17	1.85e-12	Review	298-2500	2
$C_3H_8 + NO_3 \rightarrow C_3H_7 + HNO_3$	4.17e-12	0	3260.6		[19]	7.44e-17	1.22e-13	Theory	298	2
$C_3H_8 + NO_2 \rightarrow C_3H_7 + HONO$	4.00e-13	0	11400		[20]	9.89e-30	1.73e-18	Expt	423-498	2
$C_3H_8 + O_3 \rightarrow Products$	2.74e-13	0	7270		[21]	7.05e-24	1.04e-16	Expt	273-333	2
$C_3H_8 + OH \rightarrow C_3H_7 + H_2O$	1.44e-12	1	130		[22]	9.25e-13	3.85e-12	Review	300-1000	2

$C_3H_7 + O \rightarrow Products$	1.6e-10	0	0				[18]	1.60e-10	1.60e-10	Review	300-2500	2
$CO + O \rightarrow CO_2$	1.70e-33	0	1509	1e-14	0	1629	[5]	8.86e-18	5.55e-16	Review	300-2500	3

**See discussion of more complicated rate expression that was used in the original reference

Reactions used in N₂O₅ box model

Reaction	Rate Expression											
	A ₀	n 0	Ea/R ₀	A∞	n∞	Ea/R _∞	Ref.	k(298K)	k(950K)	Technique	Temp range	Order
$NO_3 + NO_2 \rightarrow N_2O_5$	2.0e-30	-4.4	0	1.4e-12	-0.7	0	[2]	1.17e-12	5.66e-14	Expt	~250-400	3
$NO_2 + O \rightarrow NO_3$	2.50e-31	-1.8	0	2.2e-11	-0.7	0	[2]	2.84e-12	1.72e-13	Expt	~200-400	3
$NO + O \rightarrow NO_2$	9.00e-32	-1.5	0	3.00e-11	0	0	[2]	1.36e-12	9.33e-14	Expt	~200-500	3
$O_2 + O \rightarrow O_3$	6.00e-34	-2.4	0	0	0	0	[2]	1.21e-14	2.44e-16	Expt	~200-270	3
$O + O \rightarrow O_2$	5.21e-35	0	-900				[5]	2.13e-14	8.33e-16	Review	200-4000	3
$N_2O_5 \rightarrow NO_2 + NO_3$	1.30e-3	-3.5	11000	9.7e14	0.1	11080	[8]	0.0267	10000	Expt	200-400	2
$NO_3 + NO \rightarrow 2NO_2$	1.79e-11	0	-109.45				[9]	2.60e-11	2.02e-11	Review	220-4400	2
$NO_3 + O \rightarrow O_2 + NO_2$	1.00e-17	0	0				[2]	1.00e-11	1.00e-11	Expt	298	2
$NO_2 + O \rightarrow NO + O_2$	5.10e-12	0	-210				[2]	1.04e-11	6.40e-12	Expt	~200-350	2
$NO_2 + O_3 \rightarrow NO_3 + O_2$	1.2e-13	0	2450				[2]	2.82e-17	8.44e-15	Expt	~250-350	2
$NO + O_3 \rightarrow NO_2 + O_2$	3.00e-12	0	1500				[2]	1.80e-14	5.91e-13	Expt	~200-450	2
$O_3 \rightarrow O + O_2$	7.16e-10	0	11200	N/A	N/A	N/A	[4]	3.48e-07	10000	Review	300-3000	2
$O \rightarrow Walls$			7(0 s ⁻¹			*see main text*					
$NO_3 \rightarrow NO_2 + O$						*se	ee main text*					

Reactions used in NH₃ box model

Reaction			Rate E	xpression								
	A ₀	n ₀	Ea/R ₀	A∞	n∞	Ea/R∞	Ref.	k(298K)	j(950K)	Technique	Temp range	Order
$HNO \rightarrow NO + H$	5.48e-7	-1.24	25257	N/A	N/A	N/A	[3]	9.75e-32	1.076	Review	300-2500	2
$NH_3 + O \rightarrow NH_2 + OH$	2.87e-13	2.1	0				[23]	6.04e-18	3.00e-13	Review	298-2000	2
$NH_3 + OH \rightarrow NH_2 + H_2O$	4.48e-13	1.8	0				[24]	1.16e-13	2.58e-12	Review	225-2350	2
$NH_2 + O_3 \rightarrow NH_2O + O_2$	4.9e-12	0	1000				[25]	8.71e-14	1.66e-12	Review	250-380	2
$NH_2 + O \rightarrow HNO + H$	7.47e-11	0	0				[23]	7.47e-11	7.47e-11	Review	298-3000	2
$NH_2 + O \rightarrow OH + NH$	1.16e-11	0	0				[23]	1.16e-11	1.16e-11	Review	298-3000	2
$NH_2 + O \rightarrow NO + H_2$	8.30e-12	0	0				[23]	8.30e-12	8.30e-12	Review	298-3000	2
$NH_2 + NH_2 \rightarrow N_2H_4$	1.96e-29	-3.9	0	N/A	N/A	N/A	[26]	1.12e-10	1.60e-10	Expt	200-400	3
$NH_2 + OH \rightarrow NH_2OH$	6.77e-10	-3.23	673				[27]	8.30e-11	8.65e-12	Theory	200-3000	2
$NH_2 + OH \rightarrow NH + H_2O$	7.69e-13	1.5	-230				[23]	1.46e-12	5.33e-12	Review	250-3000	2
$NH_2 + OH \rightarrow NH_3 + O$	4.95e-15	2.6	-870				[23]	1.01e-13	2.36e-13	Review	298-2000	2
$NH_2 + NH \rightarrow N_2H_2 + H$	1.5e-10	-0.27	-38.4				[28]	1.84e-10	1.15e-10	Theory	200-2500	2
$NH_2 + NH_2OH \rightarrow NH_3 + NH_2O$	1.42e-15	4	-13.03				[28]	7.01e-16	1.29e-13	Theory	300-2500	2
$NH_2O + O_3 \rightarrow Products$	2.01e-14	0	0				[29]	2.01e-14	2.01e-14	Expt	298	2
$NH_2O + OH \rightarrow H_2O + HNO$	1.66e-12	0	0				[30]	1.66e-12	1.66e-12	Theory	80-420	2

$NH_2OH \rightarrow OH + NH_2$	0.16	-5.96	33555				[28]	2.09e-40	0.195	Theory	450-2500	2	
$NH + OH \rightarrow HNO + H$	3.32e-11	0	0				[23]	3.32e-11	3.32e-11	Review	298-3000	2	
$NH_2OH + NH \rightarrow NH_2 + NH_2O$	3.73e-16	4.4	786.6				[28]	6.82e-18	2.24e-14	Theory	400-2500	2	
$NO + O \rightarrow NO_2$	9.00e-32	-1.5	0	3.00e-11	0	0	[2]	1.93e-12	9.33e-14	Expt	~200-500	3	
$NO + O_3 \rightarrow NO_2 + O_2$	3.00e-12	0	1500				[2]	7.11e-15	5.91e-13	Expt	~200-400	2	
$NO_2 + O \rightarrow NO_3$	5.10e-12	0	-210				[2]	4.00e-12	4.00e-12	Expt	~200-400	3	
$NO_2 + O_3 \rightarrow NO_3 + O_2$	1.2e-13	0	2450				[2]	6.19e-18	8.44e-15	Expt	~250-350	2	
$NO_3 \rightarrow NO_2 + O$		**See main text											
$NO + H \rightarrow HNO$	1.22e-31	-1.17	211.6	N/A	N/A	N/A	[2]	1.46e-12	1.57e-13	Expt	230-4200	3	
$O_3 \rightarrow O + O_2$	7.16e-10	0	11200	N/A	N/A	N/A	[4]	4.02e-10	10000	Review	300-3000	2	
$NO_3 + NO \rightarrow NO_2 + NO_2$	1.79e-11	0	-109.45				[9]	2.78e-11	2.02e-11	Review	220-4400	2	
$NO_3 + O \rightarrow O_2 + NO_2$	1.00e-17	0	0				[2]	1.00e-11	1.00e-11	Expt	298	2	
$NO_3 + OH \rightarrow HO_2 + NO_2$	2.2e-11	0	0				[2]	2.20e-11	2.20e-11	Expt	298	2	
$HNO + H \rightarrow NH_2 + O$	1.05e-9	-0.3	14673				[23]	2.32e-35	9.37e-17	Review	550-3000	2	
$HNO + H \rightarrow OH + NH$	2.41e-9	-0.5	9009				[23]	4.66e-25	8.19e-14	Review	350-3000	2	
$HNO + H \rightarrow H_2 + NO$	3.01e-11	0	500				[3]	4.01e-12	1.75e-11	Review	298-2000	2	
$O + HNO \rightarrow OH + NO$	6.00e-11	0	0				[3]	6.00e-11	6.00e-11	Review	298-2000	2	
$OH + HNO \rightarrow H_2O + NO$	8.00e-11	0	500				[3]	1.07e-11	4.65e-11	Review	300-2000	2	
$NH_2 + NO \rightarrow N_2 + H_2O$	5.96e-11	-2.37	436				[31]	1.61e-11	2.59e-12	Review	400-1900	2	
$NH_2 + NO_2 \rightarrow N_2O + H_2O$	7e-12	-1.44	135				[32]	5.34e-12	1.20e-12	Expt	300-910	2	
$NH_2 + \overline{NO_2} \rightarrow NO + NH_2O$	5.81e-12	0	0				[33]	5.81e-12	5.81e-12	Expt	850-1350	2	
$O \rightarrow Walls$			~7	'0 s ⁻¹			**See main text						
$OH \rightarrow Walls$			~4	-6 s ⁻¹			**See main text						

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